

## **A Study of the Formation of $\text{CuAl}_2\text{O}_4$ from $\text{CuO}$ and $\text{Al}_2\text{O}_3$ by Solid State Reaction at $1000^\circ\text{C}$ and $950^\circ\text{C}$**

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With 3 Figures

**Abstract.** The formation of the spinel  $\text{CuAl}_2\text{O}_4$  from the oxides  $\text{CuO}$  and  $\text{Al}_2\text{O}_3$  has been studied at  $1000$  and  $950^\circ\text{C}$  in air by measuring the fraction reaction completed as a function of time. In the experiments the molar oxide ratios were  $\text{CuO}/\text{Al}_2\text{O}_3 = 0.5, 1.0$  and  $2.0$  and the grain size for  $\text{CuO}$  was  $1-3\ \mu$  throughout while for  $\text{Al}_2\text{O}_3$  fractions of  $40-60\ \mu$ ,  $71-100\ \mu$  and  $100-125\ \mu$ , were used. The rate of reaction could be explained quite well assuming a three-dimensional diffusion mechanism.

Über die Bildung von  $\text{CuAl}_2\text{O}_4$  aus  $\text{CuO}$  und  $\text{Al}_2\text{O}_3$  durch Reaktion im festen Zustand bei  $1000$  und  $950^\circ\text{C}$

**Inhaltsübersicht.** Die Bildung des Spinells  $\text{CuAl}_2\text{O}_4$  aus den Oxiden  $\text{CuO}$  und  $\text{Al}_2\text{O}_3$  ist bei  $1000$  und  $950^\circ\text{C}$  in der Luft untersucht worden. Die Umsetzung der Oxide in Spinell wurde als Funktion der Zeit gemessen. Während der Experimente waren die Molbrüche  $\text{CuO}/\text{Al}_2\text{O}_3 = 0.5, 1.0$  und  $2.0$ . Die Korngröße des  $\text{CuO}$  war durchgehend  $1-3\ \mu$ , dagegen wurden für  $\text{Al}_2\text{O}_3$  folgende Fraktionen verwendet:  $40-60\ \mu$ ,  $71-100\ \mu$  und  $100-125\ \mu$ . Die Reaktionsgeschwindigkeit konnte unter der Annahme eines Diffusionsmechanismus erklärt werden.

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### **Introduction**

Pure  $\text{Al}_2\text{O}_3$  in sintered form is very often used in high temperature studies as a resistant material, e. g. in tubes, crucibles and vessels. Despite its frequent use in high temperature work, from a thermodynamic point of view  $\text{Al}_2\text{O}_3$  is in fact not stable in contact with many metal oxides. In other circumstances a rapid reaction is desired between  $\text{Al}_2\text{O}_3$  and the metal oxide, e. g. in forming various spinels. Whatever the case, it is desirable to know more about the factors which influence the speed of reaction between  $\text{Al}_2\text{O}_3$  and metal oxides.

Because of our interest in various Cu-systems<sup>1)2)</sup> it was natural to choose  $\text{CuO}$  as the metal oxide component in this connection. At temperatures

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<sup>1)</sup> G. ERIKSSON and E. ROSÉN, Acta polytechn. scand., Chem. includ. Metallurgy Ser. 99, 3 (1971).

<sup>2)</sup> G. ERIKSSON and E. ROSÉN, Scand. J. Met. 2, 95 (1973).

below  $1026^\circ\text{C}$  and in air the product formed is the spinel  $\text{CuAl}_2\text{O}_4$ <sup>3)</sup>. In the present investigation of the formation of  $\text{CuAl}_2\text{O}_4$  from the oxide components  $\text{Al}_2\text{O}_3$  and  $\text{CuO}$ , the influence of temperature, particle size and ratio of initial oxides was studied and the rate controlling reaction mechanism was established.

A limited study of this reaction was earlier performed by STONE and TILLEY<sup>4)</sup> at  $900$  and  $960^\circ\text{C}$ .

## Experimental

**Method.** To determine the fraction of conversion of the oxide components  $\text{CuO}$  and  $\text{Al}_2\text{O}_3$  to  $\text{CuAl}_2\text{O}_4$ , the "single-pellet technique" was used. The samples were prepared by carefully mixing the oxides and pressing to form pellets. The pellets were placed in alumina crucibles and put into a furnace kept at  $1000$  or  $950^\circ\text{C}$ . After various reaction times a pellet was removed and quenched, finely ground and, finally, the amount of unreacted  $\text{CuO}$  was determined by electrolytic Cu-determination in the solution obtained by dissolving the residual  $\text{CuO}$  in dilute acid.

**Chemicals.** The starting materials,  $\text{CuO}$  (Merck, p. a.) and  $\text{Al}_2\text{O}_3$  (Fischer, p. a.) were heated 24 hours at  $1000^\circ\text{C}$  and 120 hours at  $1200^\circ\text{C}$  respectively. To establish the cell parameters, powder photographs were taken with  $\text{CuK}_{\alpha 1}$ -radiation in a GUINIER-HÄGG type camera ( $\lambda = 1.54051 \text{ \AA}$ ) with  $\text{Pb}(\text{NO}_3)_2$  ( $a = 7.8575 \text{ \AA}$ ) as internal standard. The cell parameter values obtained at  $25^\circ\text{C}$  are: for  $\text{CuO}$  (with monoclinic symmetry)  $a = 4.6886(3) \text{ \AA}$ ,  $b = 3.4231(2) \text{ \AA}$ ,  $c = 5.1037(4) \text{ \AA}$ ,  $\beta = 99.574(6)^\circ$  and for  $\text{Al}_2\text{O}_3$  (with hexagonal symmetry)  $a = 4.7606(4) \text{ \AA}$ ,  $c = 12.9970(16)$ . These parameter values are in good agreement with corresponding values given in the literature<sup>5)6)</sup>.

To check which phases are formed in the reaction, pure  $\text{CuAl}_2\text{O}_4$  was also prepared and investigated by powder X-ray. The spinel  $\text{CuAl}_2\text{O}_4$  was synthesized by the intimate mixing of  $\text{CuO}$  and  $\text{Al}_2\text{O}_3$  in the required proportions and heating the pellets at  $1000^\circ\text{C}$  for about 100 hours with several intermediate grindings. A slight excess of  $\text{CuO}$  was used and then removed by dissolution in dilute nitric acid. The observed values of  $\sin^2 \Theta$  and of relative intensities,  $I$ , are given in Table 1.

The intensities were visually estimated following the 6-fold scale: ss = very strong, s = strong, m = medium, w = weak, vw = very weak, vvw = extremely weak. In Table 1 are also given the calculated quantities  $d_{\text{calc}}$  and  $\Delta = (\sin^2 \Theta_{\text{obs}} - \sin^2 \Theta_{\text{calc}})$ . The cell parameter value obtained was  $a = 8.0788(2) \text{ \AA}$ , in excellent agreement with the value  $a = 8.078 \pm 0.001 \text{ \AA}$  recently given by COOLEY and REED<sup>7)</sup>.

<sup>3)</sup> A. M. M. GADALLA and J. WHITE, Trans. Brit. ceram. Soc. **63**, 39 (1964).

<sup>4)</sup> F. S. STONE and R. J. D. TILLEY, Reactivity of Solids, G.-M. SCHWAB (ed.), 5th Intern. Symposium, Munich 1964.

<sup>5)</sup> S. ÅSBRINK and L.-J. NORRBY, Acta crystallogr. [Copenhagen] **B 26**, 8 (1971).

<sup>6)</sup> J. P. JAN, S. STEINEMANN and P. DINICHERT, Physics and Chemistry of Solids **12**, 349 (1960).

<sup>7)</sup> R. F. COOLEY and J. S. REED, J. Amer. ceram. Soc. **55**, 395 (1972).

Table 1 X-ray powder diffraction data for  $\text{CuAl}_2\text{O}_4$  at  $25^\circ\text{C}$  taken with  $\text{CuK}\alpha_1$ -radiation ( $\lambda = 1.54051 \text{ \AA}$ ) and using  $\text{Pb}(\text{NO}_3)_2$  ( $a = 7.8575 \text{ \AA}$ ) as internal standard

$hkl$	$I_{\text{obs}}$	$\sin^2 \theta_{\text{obs}}$	$\Delta \cdot 10^4$	$d_{\text{calc}}, \text{\AA}$
1 1 1	vw	0.02740	13	4.6643
2 2 0	s	0.07278	6	2.8563
3 1 1	ss	0.10001	1	2.4358
4 0 0	m	0.14547	2	2.0197
3 3 1	vw	0.17269	-3	1.8534
4 2 2	m	0.21813	-3	1.6491
5 1 1	s	0.24546	2	1.5548
4 4 0	ss	0.29094	5	1.4281
6 2 0	m	0.36356	-5	1.2774
5 3 3	m	0.39081	-8	1.2320
6 2 2	vw	0.39997	-0	1.2179
4 4 4	w	0.43647	13	1.1661
7 1 1	vw	0.46355	-6	1.1313

**Preparation of samples.** The pre-heated  $\text{CuO}$  was wet-ground in a mill to a grain size of  $1-3 \mu$  ( $\mu = 10^{-6} \text{ m}$ ). The calcined  $\text{Al}_2\text{O}_3$  was passed through sieves into several fractions and those representing the sieve openings (d)  $40-63 \mu$ ,  $71-100 \mu$  and  $100-125 \mu$  were used in the experiments. Optical observations indicated that the  $\text{Al}_2\text{O}_3$ -grains were fairly spherical in form. After drying and weighing, pellets were pressed from the oxide mixture with a specified  $\text{CuO}/\text{Al}_2\text{O}_3$  composition ratio. The pellets were fabricated with a pressure of about  $200 \text{ kp/cm}^2$ , had a diameter of  $13 \text{ mm}$  and were  $2-3 \text{ mm}$  thick.

Analysis showed that the initial oxide composition ratio remained constant throughout the various operations.

**Heating procedure.** The samples were heated in a ceramic furnace of conventional form, equipped with a temperature regulator. To obtain a more uniform and stable temperature around the samples, an inner compartment was built with ceramic bricks (c. f. Fig. 1). With this arrangement the reaction temperature could be kept within  $\pm 2^\circ\text{C}$ . The pellets were placed in individual boats of recrystallized  $\text{Al}_2\text{O}_3$ . These boats with their samples were removed from the furnace at various times and quenched in air.

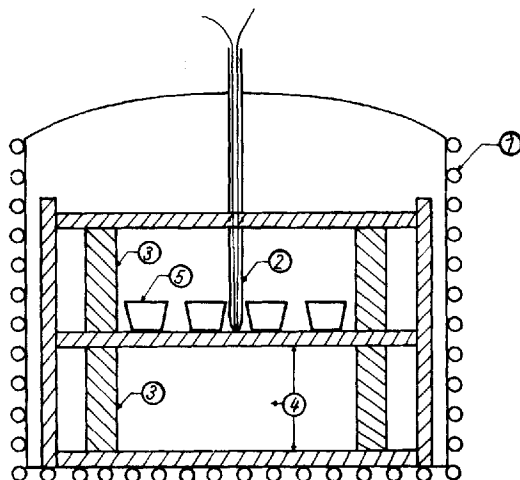


Fig. 1. Sketch of the reactor. 1 Heating windings; 2 Pt-Pt (10% Rh) thermocouple; 3 Ceramic stones; 4 Square plates of sillimanite; 5 Alumina crucibles for samples

The temperature was measured with a Pt—Pt (10% Rh) thermocouple and the emf obtained was measured with a precision potentiometer (Leeds and Northrup, K 3 Universal Potentiometer).

**Analysis.** It was found that  $\text{CuO}$  rapidly and totally dissolves in a dilute nitric acid solution, while  $\text{Al}_2\text{O}_3$  and  $\text{CuAl}_2\text{O}_4$  are insoluble. A quenched pellet was ground, a sample of about 500 mg was put in a beaker containing 25 ml dilute  $\text{HNO}_3$  (0.9 M) and  $\text{H}_2\text{SO}_4$  (0.75 M) and boiled for about 90 minutes. After cooling and sedimentation for about 60 minutes an electrolytic determination of copper was performed. In control experiments starting with pure  $\text{CuAl}_2\text{O}_4$  no copper could be detected.

From stoichiometric considerations it can be shown that the quantity  $\alpha$  (the relative molar amount of  $\text{CuAl}_2\text{O}_4$  formed) can be calculated according to the relation

$$\alpha = \frac{n_{\text{CuAl}_2\text{O}_4}}{n_{\text{CuAl}_2\text{O}_4}^{\text{max}}} = \frac{n_{\text{CuO}}^* - n_{\text{CuO}}}{n_{\text{CuAl}_2\text{O}_4}^{\text{max}}} \quad (1)$$

Here  $n$  stands for the number of moles at an arbitrary time  $t$  and the superscript  $*$  indicates the condition in the initial mixture ( $t = 0$ ). The quantity  $n_{\text{CuAl}_2\text{O}_4}^{\text{max}}$  is the maximum amount of the spinel  $\text{CuAl}_2\text{O}_4$  which can possibly be formed. Thus, in cases  $n_{\text{CuO}}^* \leq n_{\text{Al}_2\text{O}_3}^*$ ,  $n_{\text{CuAl}_2\text{O}_4}^{\text{max}} = n_{\text{CuO}}^*$  and in cases  $n_{\text{CuO}}^* \geq n_{\text{Al}_2\text{O}_3}^*$ ,  $n_{\text{CuAl}_2\text{O}_4}^{\text{max}} = n_{\text{Al}_2\text{O}_3}^*$ .

In the electrolytic determination the amount of copper deposited ( $W_{\text{Cu}}$ ) and  $n_{\text{CuO}}$  is calculated according to the relation

$$n_{\text{CuO}} = n_{\text{Cu}} = \frac{W_{\text{Cu}}}{M_{\text{r}}(\text{Cu})} \quad (2)$$

where  $M_{\text{r}}(\text{Cu})$  is the relative molecular mass of copper.

## Results and Discussion

The results obtained for  $\alpha$  at various reaction times with different values for the parameters considered, i. e. temperature, particle size and the oxide ratio  $n_{\text{CuO}}^*/n_{\text{Al}_2\text{O}_3}^*$ , are given in Table 2 and plotted in Figs. 2 and 3. At 1000°C an effort was made to choose reaction times in such a way that the resultant  $\alpha$ -values were rather evenly distributed from 0 to 100% while at 950°C only  $\alpha$ -values less than 30% were obtained.

In order to determine the rate controlling reaction mechanism, the  $\alpha$ -values obtained at 1000°C were plotted against  $t/t_{0.5}$  (c. f. Fig. 3), where  $t_{0.5}$  indicates the time for 50% reaction. The feature of this curve can indicate the type of reaction mechanism by comparison with the calculated curves representing different types of idealized reaction mechanisms<sup>8)</sup>. As seen from Fig. 3 the experimental data agree quite well with the curve valid for a three-dimensional diffusion mechanism and significantly deviate from curves representing other types of rate controlling reaction mechanisms, e. g. a phase-boundary mechanism.

<sup>8)</sup> J. H. SHARP, G. W. BRINDLEY and B. N. NARAHARI ACHAR, J. Amer. ceram. Soc. **49**, 379 (1966).

Table 2 Amount of  $\text{CuAl}_2\text{O}_4$  formed (in mole percentage) at various reaction times for different values on the oxide ratio  $\text{CuO}/\text{Al}_2\text{O}_3$  and for different particle sizes

mole ratio	$d_{\text{Al}_2\text{O}_3}, \mu$	reaction time, h	$\alpha \cdot 100$
a) Measurements at 1000°C			
1.0022	40-63	0.50	$4.30 \pm 0.18$
		1.00	$5.78 \pm 0.34$
		2.00	$9.69 \pm 0.07$
		4.00	$17.99 \pm 0.14$
		10.00	$34.85 \pm 0.23$
		21.17	$51.02 \pm 0.04$
		67.25	$74.41 \pm 0.37$
0.9979	71-100	0.50	$3.37 \pm 0.05$
		1.00	$4.77 \pm 0.19$
		2.00	$9.19 \pm 0.19$
		4.00	$18.71 \pm 0.18$
		10.00	$31.74 \pm 0.11$
		21.17	$44.70 \pm 0.10$
		67.25	$64.68 \pm 0.07$
0.9979	100-125	0.50	$1.34 \pm 0.23$
		1.00	$2.74 \pm 0.10$
		2.00	$6.20 \pm 0.01$
		4.00	$11.91 \pm 0.22$
		10.00	$22.28 \pm 0.33$
		21.17	$32.72 \pm 0.08$
		67.25	$52.65 \pm 0.07$
0.5008	71-100	0.50	$4.20 \pm 0.11$
		1.00	$7.43 \pm 0.02$
		2.00	$16.03 \pm 0.10$
		4.00	$29.63 \pm 0.02$
		10.00	$51.60 \pm 0.06$
		21.17	$71.41 \pm 0.07$
		67.25	$86.24 \pm 0.02$
2.0053	71-100	0.50	$3.07 \pm 0.01$
		1.00	$5.23 \pm 0.40$
		2.00	$9.81 \pm 0.65$
		4.00	$18.31 \pm 0.06$
		10.00	$33.37 \pm 0.01$
		21.17	$48.77 \pm 0.19$
		67.25	$72.50 \pm 0.08$
b) Measurements at 950°C			
0.9979	71-100	2.00	$1.43 \pm 0.11$
		4.00	$3.33 \pm 0.31$
		8.00	$5.34 \pm 0.15$
		16.00	$9.57 \pm 0.26$
		32.00	$19.40 \pm 0.05$
		64.00	$27.21 \pm 0.25$

In order to more carefully analyse the diffusion-controlled reaction, the VALENSI-CARTER<sup>9)</sup> model was considered

$$\frac{Z}{Z-1} - (1-\alpha)^{2/3} - \frac{1}{Z-1} [1 + (Z-1)\alpha]^{2/3} = \frac{2k \cdot t}{r_0^2} \quad (3)$$

<sup>9)</sup> R. E. CARTER, J. physic. Chem. **34**, 2010 (1961).

where  $k$  is the rate constant,  $r_0$  the mean particle size and  $Z$  is a term accounting for the relative change in molar volume,  $V$  in  $\text{cm}^3 \text{mole}^{-1}$  (the  $V$ -values used were taken from the literature)

$$Z = V_{\text{CuAl}_2\text{O}_4} / V_{\text{Al}_2\text{O}_3} = 1.15$$

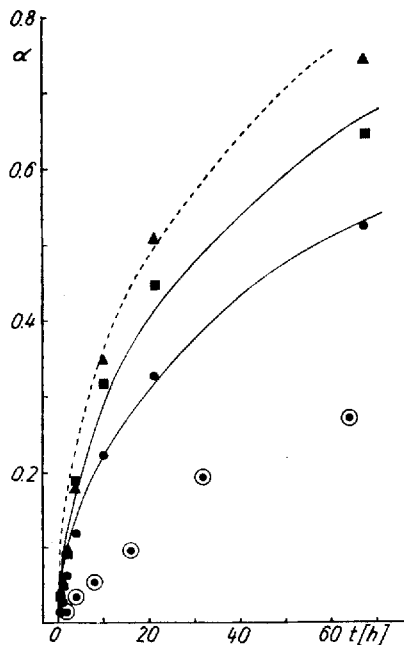


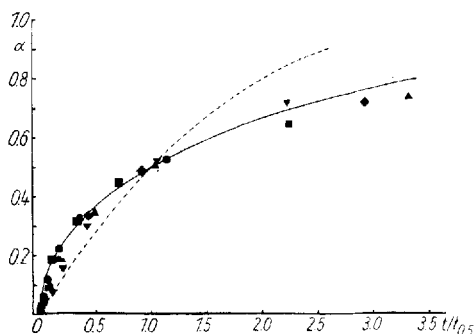
Fig. 2. Amount of  $\text{CuAl}_2\text{O}_4$  formed ( $\alpha$ ) as a function of reaction time for the oxide ratio  $\text{CuO}/\text{Al}_2\text{O}_3 = 1.0$   
 $\blacktriangle$   $d = 40-63 \mu$ ,  $T = 1000^\circ\text{C}$ ;  $\blacksquare$   $d = 71-100 \mu$ ,  $T = 1000^\circ\text{C}$ ;  $\bullet$   $d = 100-125 \mu$ ,  $T = 1000^\circ\text{C}$ ;  
 $\bigcirc$   $d = 71-100 \mu$ ,  $T = 950^\circ\text{C}$

The curves at  $1000^\circ\text{C}$  are calculated using eq. (3) and with the rate constant value  $k = 1.1 \cdot 10^{-8} \text{ cm}^2 \text{ h}^{-1}$  (full-drawn curves) and  $k = 0.6 \cdot 10^{-8} \text{ cm}^2 \text{ h}^{-1}$  (broken curve)

Fig. 3. Amount of  $\text{CuAl}_2\text{O}_4$  formed ( $\alpha$ ) as a function of reduced reaction time,  $t/t_{0.5}$ , at  $T = 1000^\circ\text{C}$ .

$\blacktriangle$   $d = 40-63 \mu$ ,  $\text{CuO}/\text{Al}_2\text{O}_3 = 1.00$ ;  
 $\blacksquare$   $d = 71-100 \mu$ ,  $\text{CuO}/\text{Al}_2\text{O}_3 = 1.00$ ;  
 $\bullet$   $d = 100-125 \mu$ ,  $\text{CuO}/\text{Al}_2\text{O}_3 = 1.00$ ;  
 $\blacktriangledown$   $d = 71-100 \mu$ ,  $\text{CuO}/\text{Al}_2\text{O}_3 = 0.50$ ;  
 $\blacklozenge$   $d = 71-100 \mu$ ,  $d \text{ CuO}/\text{Al}_2\text{O}_3 = 2.00$ .

The broken curve is valid for a phase-boundary reaction mechanism while the full-drawn curve for a diffusion-controlled reaction mechanism.



From the CARTER plot (or equally well from numerical calculations) a value on the ratio  $2k/r_0^2$  can be obtained. Assuming the particles have a rectangular distribution, for the ratio  $n_{\text{CuO}}^*/n_{\text{Al}_2\text{O}_3}^* = 1.0$  values on the rate constant were calculated for each fraction. For the fractions  $71-100 \mu$  and  $100-125 \mu$  the experimental data could be explained quite well with

a rate constant value  $k = 1.1 \cdot 10^{-8} \text{ cm}^2 \text{ h}^{-1}$  (see Fig. 2), while for the fraction 40–60  $\mu$  a somewhat lower value,  $k = 0.6 \cdot 10^{-8} \text{ cm}^2 \text{ h}^{-1}$ , was obtained. The spread in the  $k$ -values may be due mainly to irregularities in the shapes and sizes of the particles from one fraction to the other. The corresponding rate values obtained for the fraction 71–100  $\mu$  and  $n_{\text{CuO}}^*/n_{\text{Al}_2\text{O}_3}^* = 0.5$  and 2.0, were  $k = 1.7 \cdot 10^{-8} \text{ cm}^2 \text{ h}^{-1}$  and  $k = 4.4 \cdot 10^{-8} \text{ cm}^2 \text{ h}^{-1}$  respectively, indicating that for equal molar ratios of the two oxides, the reaction rate is minimal and increases when an excess of either oxide is present.

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